Code: 20ME3501

## III B.Tech - I Semester - Regular Examinations - DECEMBER 2022

## HEAT TRANSFER (MECHANICAL ENGINEERING)

## Duration: 3 hours

Max. Marks: 70
Note: 1. This paper contains questions from 5 units of Syllabus. Each unit carries 14 marks and have an internal choice of Questions.
2. All parts of Question must be answered in one place.

BL - Blooms Level
CO - Course Outcome

|  |  |  | BL | CO | Max. <br> Marks |
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| UNIT-I |  |  |  |  |  |
| 1 | a) | Derive a general heat conduction equation in rectangular coordinate system. | L2 | CO1 | 7 M |
|  | b) | A plane wall is 150 mm thick and its wall area is $4.5 \mathrm{~m}^{2}$. Its conductivity is $9.35 \mathrm{~W} / \mathrm{m}-\mathrm{K}$ and temperatures are steady at $150^{\circ} \mathrm{C}$ and $45^{\circ} \mathrm{C}$ on both sides. Determine the heat transfer rate in flow direction. | L2 | CO1 | 7 M |
| OR |  |  |  |  |  |
| 2 | a) | Derive a three-dimensional generalized heat conduction equation in a cylindrical coordinate system. | L2 | CO1 | 7 M |
|  | b) | List out the applications of heat transfer in various fields. | L2 | CO1 | 7 M |
| UNIT-II |  |  |  |  |  |
| 3 | a) | Derive the expression for heat transfer in case of a rectangular plate fin of uniform cross section with insulated end. | L3 | CO 2 | 7 M |
|  | b) | What are heisleir charts? Under what conditions heislier charts are used in heat transfer problems. | L3 | CO 2 | 7 M |

## OR

| 4 | a) | Two fins are identical except the diameter <br> of one is twice that of the other. Compare <br> their efficiencies and effectiveness. | L 3 | CO 2 | 7 M |
| :--- | :--- | :--- | :--- | :--- | :--- |
| b) | A 1.0 mm diameter wire is maintained at a <br> temperature of $400^{\circ} \mathrm{C}$ and exposed to a <br> convective environment at $40^{\circ} \mathrm{C}$ with <br> h=50W/m ${ }^{2} \mathrm{~K}$. Calculate thermal <br> conductivity which just causes an insulation <br> thickness of 0.2 mm produce a critical <br> radius. How much of this insulation must be <br> added to reduce the heat transfer by $75 \%$. | CO |  |  |  |


| UNIT-III |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| 5 | a) | Using Buckingham $\Pi$-Theorem obtain relation for natural convection in terms of dimensionless numbers. | L3 | CO 2 | 7 M |
|  | b) | Water at $38^{\circ} \mathrm{C}$ flows over a wide, 6 m long, heated plate at $0.06 \mathrm{~m} / \mathrm{s}$. For a surface temperature of $93^{\circ} \mathrm{C}$, determine: <br> i. The hydrodynamic boundary layer thickness $\delta$ at the end of the plate. <br> ii. The total drag on the surface per unit width. <br> iii. The thermal boundary layer thickness $\delta_{\mathrm{t}}$ at the end of the plate. <br> $i v$. The local heat transfer coefficient $h_{x}$ at the end of the plate and <br> v. The total heat flux from the surface per unit width. | L3 | CO2 | 7 M |
| OR |  |  |  |  |  |
| 6 | a) | Explain the phenomena of natural convection over a vertical hot plate. Sketch the temperature and velocity boundary layer profiles. | L3 | CO 2 | 7 M |


|  | b) | Water flows in a duct having a cross section $5 \times 10 \mathrm{~mm}$ with a mean bulk temperature of $20^{\circ} \mathrm{C}$. If the duct wall temperature is constant at $60^{\circ} \mathrm{C}$ and fully developed laminar flow is experienced, calculate the heat transfer per unit length. | L3 | CO 2 | 7 M |
| :---: | :---: | :---: | :---: | :---: | :---: |
| UNIT-IV |  |  |  |  |  |
| 7 | a) | Explain the regimes of pool boiling. | L2 | CO3 | 7 M |
|  | b) | Saturated steam at a temperature of $65^{\circ} \mathrm{C}$ condenses on a vertical surface at $55^{\circ} \mathrm{C}$. Determine the thickness of the condensate film at locations 0.2 m and 1.0 m from the top. Also calculate condensate flow rate at these locations. | L3 | CO3 | 7 M |
| OR |  |  |  |  |  |
| 8 | a) | Derive LMTD of parallel flow and counter flow heat exchangers. | L2 | CO 3 | 7 M |
|  | b) | Refrigeration is designed to cool $250 \mathrm{~kg} / \mathrm{h}$ of hot liquids of heat $3350 \mathrm{~J} / \mathrm{kgK}$ at $120^{\circ} \mathrm{C}$ using a parallel flow arrangement. $1000 \mathrm{~kg} / \mathrm{h}$ of cooling water is available for cooling purpose at a temperature of $10^{\circ} \mathrm{C}$. If the overall heat transfer co-efficient is $1160 \mathrm{~W} / \mathrm{m}^{2} \mathrm{~K}$ and the surface area of the heat exchanger is $0.25 \mathrm{~m}^{2}$. Calculate the outlet temperature of the cooled liquid and water and also effectiveness of the heat exchanger. | L3 | CO3 | 7 M |
| UNIT-V |  |  |  |  |  |
| 9 | a) | What is Stefan-Boltzmann Law? Explain the concept of total emissive power of a surface. | L4 | CO1 | 7 M |
|  | b) | Two large parallel planes having emissivity's of 0.25 and 0.5 are maintained | L4 | CO 4 | 7 M |


|  |  | at temperatures of 1000 K and 500 K , respectively. A radiation shield having an emissivity of 0.1 is placed between the two planes. <br> Calculate <br> i. The heat-transfer rate per unit area if the shield were not present, <br> ii. The heat-transfer rate per unit area with the presence of the shield and <br> iii. The temperature of the shield. |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: |
| OR |  |  |  |  |  |
| 10 | a) | State Planck's distribution law and describe how monochromatic emissive power varies with wavelength. | L4 | CO1 | 7 M |
|  | b) | A black body of total area $0.045 \mathrm{~m}^{2}$ is completely enclosed in a sphere bounded by 5 cm thick walls. The walls have a surface area $0.5 \mathrm{~m}^{2}$ and the thermal conductivity is $1.1 \mathrm{~W} / \mathrm{m}^{\circ} \mathrm{C}$ if the inner surface of the enveloping wall is to be maintained at $215^{\circ} \mathrm{C}$ and the outer wall surface is at $30^{\circ} \mathrm{C}$ calculate the temperature of the black body. | L4 | CO4 | 7 M |

